

## Characteristics of a hydraulic jump in Bingham fluid

## Caractéristiques d'un ressaut hydraulique en fluide de Bingham

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### ABSTRACT

Hydraulic jump taking place in Bingham fluid over a horizontal plate has been studied. The formulas for conjugate depths, bottom shear stress and critical depth are established. Since no exact analytical solution in closed form can be obtained for conjugate depths, an approximate formula is developed. This formula can provide good results with an error less than 4%. The analytical results reveal that the critical depth and the ratio of conjugate depths increase until the bottom shear stress exceeds a certain value and then decrease afterwards. The bottom shear stress downstream of hydraulic jump is smaller than that upstream. The results are verified by experimental data and observations available in the literature.

### RÉSUMÉ

Un ressaut hydraulique ayant lieu dans un fluide de Bingham au-dessus d'une plaque horizontale a été étudié. On établit les formules pour les profondeurs conjuguées, le cisaillement au fond et la profondeur critique. Vu qu'aucune solution analytique exacte ne peut être obtenue sous forme fermée pour les profondeurs conjuguées, une formule approchée est développée. Cette formule peut fournir de bons résultats avec une erreur inférieure à 4%. Les résultats analytiques indiquent que la profondeur critique et le rapport des profondeurs conjuguées augmentent jusqu'à ce que l'effort de cisaillement au fond excède une certaine valeur puis diminuent ensuite. L'effort de cisaillement au fond en aval du ressaut hydraulique est plus petit que celui en amont. Les résultats sont vérifiés par des données expérimentales et des observations disponibles dans la littérature.

*Keywords:* Bingham fluid, hydraulic jump, non-Newtonian fluid.

### 1 Introduction

Muddy debris flow (Coussot, 1994a,b), a mixture of water and cohesive clay particles, behaves like an inelastic non-Newtonian fluid and is often encountered in industry and nature, e.g. sewage sludge, submarine landslides, mountain mudflows, coal slurries, drilling mud. Bingham fluid is widely used as an ideal and simple model in the study of non-Newtonian fluid. In this model, the process of cross-link formation and destruction is instantaneous. The thixotropic tendency has been ignored and the excess deviatoric stress  $\tau$  over the yield stress  $\tau_0$  is assumed to be a linear function of the strain rate  $\partial U/\partial y$  (Bingham, 1922),

$$\mu_0 \frac{\partial U}{\partial y} = \begin{cases} 0 & \text{if } |\tau| < \tau_0 \\ (\tau - \tau_0) \operatorname{sgn} \left( \frac{\partial U}{\partial y} \right) & \text{if } |\tau| \geq \tau_0 \end{cases} \quad (1)$$

where  $\mu_0$  is the fluid viscosity.

An experimental study conducted by Ogihara and Miyazawa (1994) showed that the characteristics of hydraulic jump in Bingham fluid were not able to be fully described by the classical

(Newtonian) hydraulic jump formulation. Hydraulic jump in non-Newtonian fluid was theoretically studied by Ng and Mei (1994) and Liu and Mei (1994), who provided an analysis of jump condition. Unfortunately, the analysis of conjugate depths and bottom shear stress, which are often of most interest in practical engineering, has not fully been exploited. In this paper, an adequate model for hydraulic jump in Bingham fluid has been developed. Hence, the formulas for conjugate depths, bottom shear stress and critical depth are derived. The results are compared with available experimental data.

### 2 Hydraulic jump

From the engineering viewpoint, the conjugate depths, bottom shear stress and critical depth are of primary importance in hydraulic jump. The basic equations for these characteristic quantities can be established based on the integral continuity and momentum equations, combined with the properties of Bingham fluid.

Applying the integral continuity equation, we have

$$q = \int_0^{h_1} U_1(y)dy = \int_0^{h_2} U_2(y)dy \quad (2)$$

where  $q$  is the discharge per unit width and subscripts 1 and 2 denote the upstream and downstream of hydraulic jump, respectively, for all quantities (see Figs 1 and 2).

The upstream and downstream flows of hydraulic jump taking place in Bingham fluid over a horizontal plate can be treated as two-dimensional, fully-developed, half-Poiseuille flows.  $U(y)$  in Eq. (2) can be expressed as (Liu and Mei, 1989)

$$U(\xi) = \begin{cases} U_0 & 1 - \lambda \leq \xi \leq 1 \\ U_0 \left[ 1 - \left( \frac{1 - \lambda - \xi}{1 - \lambda} \right)^2 \right] & 0 \leq \xi < 1 - \lambda \end{cases} \quad (3)$$

where  $\xi = y/h$ ,  $\lambda = \tau_0/\tau_w$ ;  $\tau_w$  is the shear stress at the bottom;  $p = \rho g(h - y)$  is the hydrostatic pressure and other symbols are shown in Fig. 1. Substitution of Eq. (3) into Eq. (2) leads to

$$\frac{1}{3}U_{01}h_1(2 + \lambda_1) = \frac{1}{3}U_{02}h_2(2 + \lambda_2). \quad (4)$$

Similarly, according to the integral momentum equation, we obtain

$$\begin{aligned} & \int_0^{h_1} \rho(\vec{V}_1 \cdot \vec{n}_1)U_1 dy + \int_0^{h_2} \rho(\vec{V}_2 \cdot \vec{n}_2)U_2 dy \\ &= \int_0^{h_1} p_1 dy - \int_0^{h_2} p_2 dy. \end{aligned} \quad (5)$$

Integrating Eq. (5) with Eq. (3) results in

$$\frac{8 + 7\lambda_2}{15}U_{02}^2h_2 - \frac{8 + 7\lambda_1}{15}U_{01}^2h_1 = \frac{g}{2}(h_1^2 - h_2^2). \quad (6)$$

Generally, the flow conditions upstream of hydraulic jump are known, i.e.  $U_{01}$ ;  $h_1$  and  $\lambda_1$ . There are two equations, Eqs (4) and (6), which obviously are not sufficient to determine the three unknowns  $U_{02}$ ;  $h_2$  and  $\lambda_2$ . An additional equation must be provided. This comes from the shear stress in Bingham fluid.

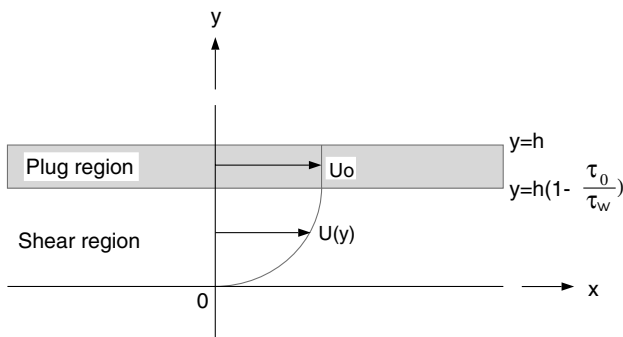


Figure 1 Velocity profile for Bingham fluid over a horizontal plate.

If Eq. (1) is applied to the upstream of hydraulic jump, we have

$$\mu_0 \frac{\partial U_1}{\partial y} \Big|_{y=0} = (\tau_1 - \tau_0)|_{y=0}. \quad (7)$$

Substitution of Eq. (3) into the above equation results in

$$\frac{2\mu_0 U_{01}}{h_1(1 - \lambda_1)} = (\tau_{w1} - \tau_0). \quad (8)$$

Similarly, we have

$$\frac{2\mu_0 U_{02}}{h_2(1 - \lambda_2)} = (\tau_{w2} - \tau_0). \quad (9)$$

Combining Eqs (8) and (9) gives

$$\frac{U_{01}h_2}{U_{02}h_1} = \frac{\lambda_2}{\lambda_1} \left( \frac{1 - \lambda_1}{1 - \lambda_2} \right)^2. \quad (10)$$

Equations (4), (6) and (10) are the basic equations for the three unknowns  $U_{02}$ ;  $h_2$  and  $\lambda_2$  for hydraulic jump in Bingham fluid.

It should be noted that there are only two unknowns,  $U_{02}$ ,  $h_2$ , for hydraulic jump in Newtonian fluid, whereas there are three,  $U_{02}$ ,  $h_2$  and  $\lambda_2$ , for hydraulic jump in Bingham or non-Newtonian fluid.

A further mathematical consideration indicates that there are no analytical solutions to the basic equations, but an asymptotic solution can be developed.

Substitution of Eq. (4) into Eqs (6) and (10), respectively, gives

$$\frac{8 + 7\lambda_2}{\eta} \left( \frac{2 + \lambda_1}{2 + \lambda_2} \right)^2 - (8 + 7\lambda_1) = \frac{5(2 + \lambda_1)^2}{6F_{r1}^2} (1 - \eta^2) \quad (11)$$

$$\eta^2 \frac{2 + \lambda_2}{2 + \lambda_1} = \frac{\lambda_2}{\lambda_1} \left( \frac{1 - \lambda_1}{1 - \lambda_2} \right)^2 \quad (12)$$

where  $\eta = h_2/h_1$  and  $F_{r1} = V_{01}/\sqrt{gh_1}$  is the Froude number, in which  $V_{01}$  is the depth-averaged velocity defined by

$$V_0 = \frac{1}{h} \int_0^h U(y) dy = \frac{1}{3}U_0(2 + \lambda). \quad (13)$$

In the present context, the hydraulic jump is a discontinuous transition from the supercritical (upstream) flow ( $F_{r1} > 1$ ) to the subcritical (downstream) flow ( $F_{r2} < 1$ ).

Combining Eq. (11) with Eq. (12) leads to a fifth-order polynomial in term of either  $\eta$  or  $\lambda_2$ . According to the algebraic field theory, there are no analytic solutions for any fifth-order polynomial. Numerical solutions will be given in Section 4.

The form of Eq. (11) suggests that an asymptotic solution can be derived in the case of  $\eta \rightarrow 1$  as follows:

Defining

$$f(\lambda_2) = \frac{8 + 7\lambda_2}{(2 + \lambda_2)^2}, \quad (14)$$

Eq. (11) becomes

$$\frac{f(\lambda_2)}{\eta} (2 + \lambda_1)^2 - (8 + 7\lambda_1) = \frac{5(2 + \lambda_1)^2}{6F_{r1}^2} (1 - \eta^2) \quad (15)$$

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With reference to Eq. (12),  $\lambda_2$  is a function of  $\eta$ . Thus  $f(\lambda_2)$  can be expanded in terms of  $(\eta - 1)$  by using the Taylor series

$$f(\lambda_2) = f(\lambda_2)|_{\eta \rightarrow 1} + \left. \frac{df(\lambda_2)}{d\eta} \right|_{\eta \rightarrow 1} (\eta - 1) + O(\eta - 1)^2. \quad (16)$$

Obviously  $\lambda_2 \rightarrow \lambda_1$  as  $\eta \rightarrow 1$ , hence

$$f(\lambda_2)|_{\eta \rightarrow 1} = f(\lambda_1). \quad (17)$$

According to the chain rule,

$$\frac{df(\lambda_2)}{d\eta} = \frac{df(\lambda_2)}{d\lambda_2} \frac{d\lambda_2}{d\eta}, \quad (18)$$

we have

$$\left. \frac{df(\lambda_2)}{d\eta} \right|_{\eta \rightarrow 1} = - \frac{(2 + 7\lambda_1)(1 - \lambda_1)\lambda_1}{(2 + \lambda_1)^2(1 + \lambda_1 + \lambda_1^2)}. \quad (19)$$

Substituting of Eqs (17) and (19) into Eq. (16) yields

$$f(\lambda_2) = \frac{8 + 7\lambda_1}{(2 + \lambda_1)^2} - \frac{(2 + 7\lambda_1)(1 - \lambda_1)\lambda_1}{(2 + \lambda_1)^2(1 + \lambda_1 + \lambda_1^2)}(\eta - 1) + O(\eta - 1)^2. \quad (20)$$

By substituting Eq. (20) into Eq. (15) and rearrangement, we obtain

$$\eta(1 + \eta) = \frac{6}{5} F_{r1}^2 \frac{8 + 17\lambda_1 + 20\lambda_1^2}{(1 + \lambda_1 + \lambda_1^2)(2 + \lambda_1)^2} [1 + O(\eta - 1)]. \quad (21)$$

By ignoring terms of order  $(\eta - 1)$  and higher, Eq. (21) becomes

$$\eta^2 + \eta - 2C_0 F_{r1}^2 = 0 \quad (22)$$

with

$$C_0 = \frac{3}{5} \frac{8 + 17\lambda_1 + 20\lambda_1^2}{(1 + \lambda_1 + \lambda_1^2)(2 + \lambda_1)^2}. \quad (23)$$

The analytical solution to Eq. (22) is

$$\eta = \frac{1}{2} [\sqrt{1 + 8C_0 F_{r1}^2} - 1]. \quad (24)$$

The energy dissipation due to hydraulic jump is referred to as the head loss  $\Delta H$ . Solving the Bernoulli (energy) equation along points on the fluid surface

$$\frac{U_{01}}{2g} + h_1 = \frac{U_{02}}{2g} + h_2 + \Delta H \quad (25)$$

and eliminating  $U_{01}$  and  $U_{02}$  yield:

$$\Delta H = (h_2 - h_1) \left[ \frac{(h_2 - h_1)^2}{4C_1 h_2 h_1} + \frac{1 - C_1}{C_1} \right] \times [1 + O(h_2 - h_1)] \quad (26)$$

where

$$C_1 = \frac{8 + 7\lambda_1}{15}. \quad (27)$$

Equation (24) is the approximate formula for the conjugate depths. Theoretically, only under the condition that  $\eta$  is close to unity, can it be valid. However, the analysis and discussion in Section 4.3 will indicate that it can be used with a good accuracy in situations where  $\eta$  is larger than unity. After  $\eta$  is obtained

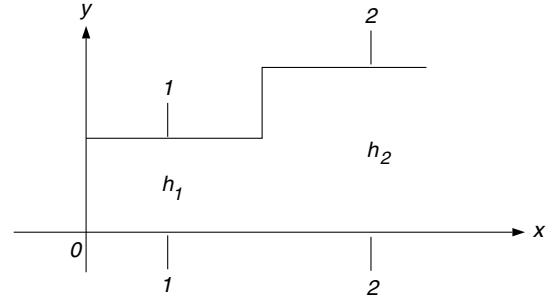


Figure 2 Sketch for a hydraulic jump.

through Eq. (24),  $U_{02}$  and  $\lambda_2$  can be calculated by Eqs (4) and (12), respectively.

It is found that  $C_0$  reaches the maximum, i.e.  $C_{0\max} = 1.22$  when  $\lambda_1 = 0.213$  or  $\tau_0/\tau_{w1} = 0.213$ . Since Bingham fluid consists of two distinct regions, plug and shear regions (Fig. 1), the existence of such maximum suggests that hydraulic jump is hereby coupled between the effects of the two regions. When  $0 \leq \lambda_1 \leq 0.213$ , the shear region dominates hydraulic jump and the relative jump height  $h_2/h_1$  is an increasing function of  $\lambda_1$ ; when  $0.213 \leq \lambda_1 \leq 1$ , the plug region dominates hydraulic jump and  $h_2/h_1$  is a decreasing function of  $\lambda_1$  (Fig. 2).

Two points are worthy mentioning. Firstly, analytical solution (24) for hydraulic jump in Bingham fluid can be extended to two extreme cases—the solution for hydraulic jump in a fully-developed Newtonian viscous flow when  $\lambda_1 = 0$  or  $C_0 = 6/5$  and that in an inviscid flow when  $\lambda_1 = 1$  or  $C_0 = 1$ . Secondly, the bottom shear stress  $\tau_{w2}$  downstream is always smaller than  $\tau_{w1}$  upstream of hydraulic jump in Bingham fluid, which becomes very clear from Eq. (12).

### 3 Critical depth

When the conjugate depths upstream and downstream of hydraulic jump are the same, such flow is referred to as a critical flow. Since approximate formula (24) becomes an exact solution when  $\eta = 1$ , the formula for critical depth is then obtained as

$$h_c = \sqrt[3]{C_0 \frac{q^2}{g}} \quad (28)$$

by setting  $\eta = 1$  and  $h_2 = h_1 = h_c$  with  $F_{r1} = q/\sqrt{gh_c^3}$  in (24). For a critical flow,  $\lambda_1 = \lambda_2 = \lambda$  in Eq. (23).

Equation (28) is the formula for the critical depth in Bingham fluid. Clearly, it is the solution for a fully viscous flow if  $\lambda = 0$  or  $C_0 = 6/5$  and that for a fully inviscid flow if  $\lambda = 1$  or  $C_0 = 1$ .  $h_c$  changes with  $\lambda$  in the interval  $0 < \lambda < 1$ . The feature of the function  $C_0$  shows that  $h_c$  increases with  $\lambda$  for  $0 \leq \lambda_1 \leq 0.213$  and decreases for  $0.213 < \lambda \leq 1$ .  $h_c$  reaches the maximum value of  $1.068 \sqrt[3]{q^2/g}$  at  $\lambda = 0.213$ , where the critical flow is coupled between the effects of plug and shear regions. The shear region dominates the critical flow in the interval  $0 \leq \lambda_1 \leq 0.213$  and the plug region dominates the flow in the interval  $0.213 < \lambda \leq 1$ . The features are also shown in Fig. 3 in terms of  $h_c/h_q$  versus  $\tau_0/\tau_w$  or  $\lambda$ , where  $h_q = \sqrt[3]{q^2/g}$ . Obviously, the critical depth

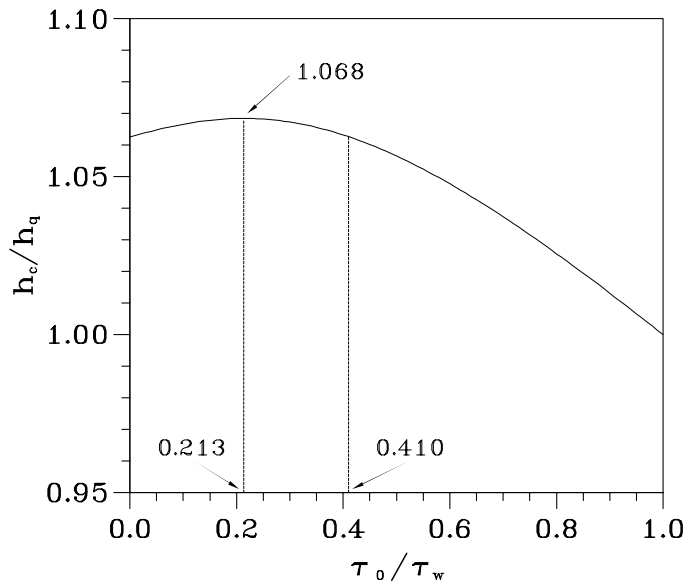


Figure 3 Critical depth versus dimensionless yield stress  $\tau_0/\tau_w$ .

is always greater than that in a fully inviscid flow, and it is also higher than that in a fully viscous flow for  $0 \leq \lambda \leq 0.41$ , but lower for  $0.41 < \lambda \leq 1$ .

#### 4 Numerical solutions of jump equations

As pointed out in Section 2, Eqs (11) and (12) cannot be solved analytically. Hence a numerical method is used to solve them. In the present study, Newton's method is applied to obtain the numerical solutions.

##### 4.1 Conjugate depths

The numerical results for the conjugate depths are plotted in Figs 4 and 5. It is clearly seen that  $\eta$  or  $h_2/h_1$  is almost a linear function of  $F_{r1}$  but is not a linear function of  $\tau_0/\tau_{w1}$  or  $\lambda_1$ .  $\eta$  always increases with  $F_{r1}$  but it may increase or decrease depending on the value of  $\lambda_1$ , which can be seen from the figures. As expected, there is one peak or maximum value of  $\eta$  as  $\lambda_1$  changes from 0 to 1.

##### 4.2 Bottom shear stress

Since  $\lambda = \tau_0/\tau_w$ ,  $\lambda$  represents the bottom shear stress  $\tau_w$ . The numerical result of  $\lambda_2$  versus  $\lambda_1$  is shown in Fig. 6. As expected,  $\lambda_2$  is always greater than  $\lambda_1$  and is an increasing function of  $\lambda_1$ . The difference between the bottom shear stresses upstream and downstream of hydraulic jump increases with  $F_{r1}$  and vanishes at  $\lambda = 0$  or 1 in which  $\lambda_2 = 0$  or 1, i.e.  $\tau_{w2} = \tau_{w1}$ .

##### 4.3 Comparison of exact and approximate results

In Section 2, an approximate formula for conjugate depths is derived for  $\eta$  close to unity. In order to examine the accuracy, a comparison between the numerical results of Eqs (11) and (12)

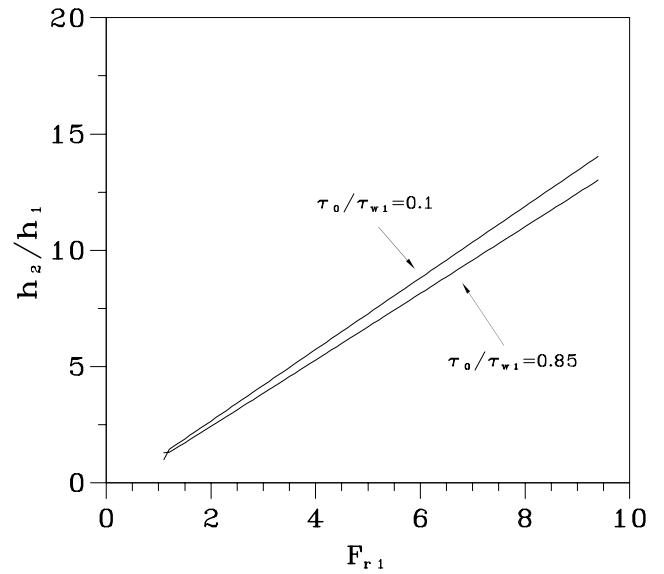


Figure 4 Conjugate depths versus Froude number  $F_{r1}$ .

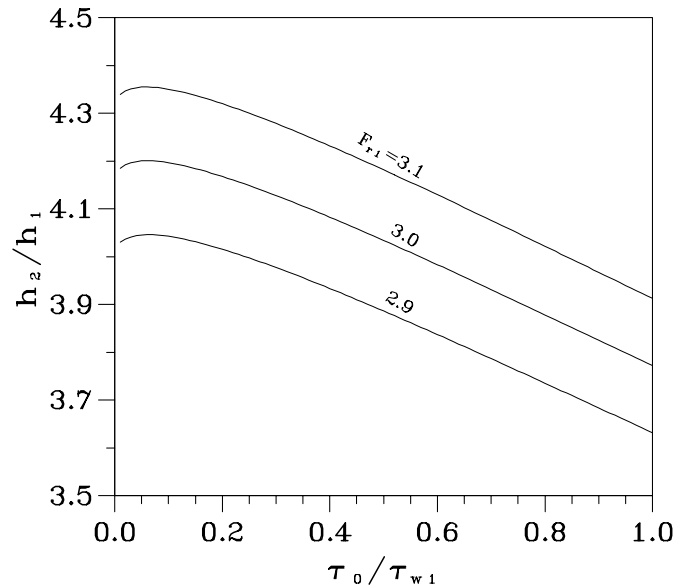


Figure 5 Conjugate depths versus dimensionless yield stress  $\tau_0/\tau_{w1}$ .

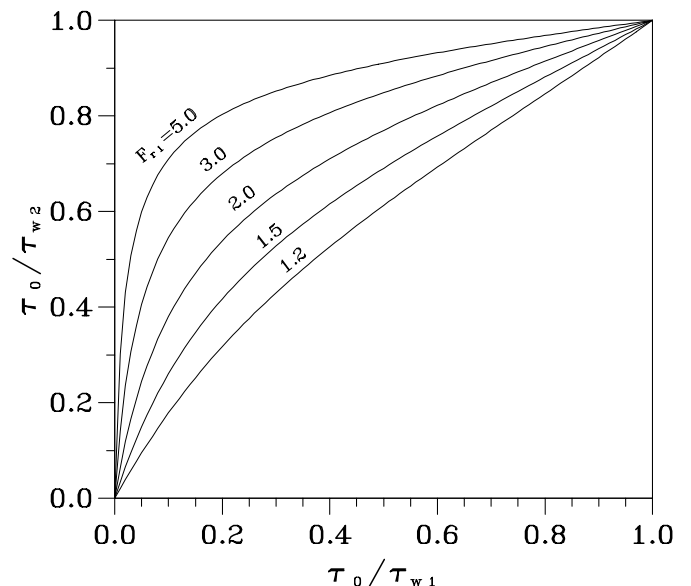


Figure 6  $\tau_0/\tau_{w2}$  versus  $\tau_0/\tau_{w1}$ .

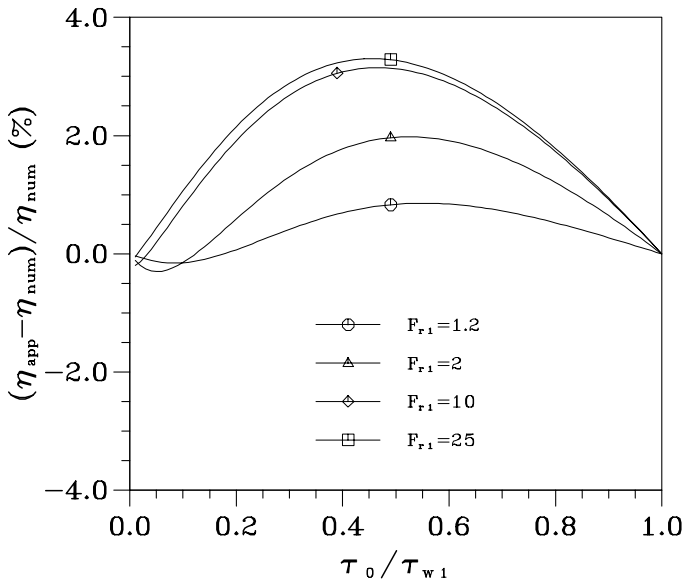


Figure 7 Relative error in percentage versus dimensionless yield stress  $\tau_0/\tau_{w1}$ .

and the approximate ones of Eq. (24) is carried out. The relative errors defined by  $(\eta|_{app} - \eta|_{num})/\eta|_{num}$ , where  $\eta|_{num}$  is calculated from Eqs (11) and (12) by numerical method and  $\eta|_{app}$  from Eq. (24), are plotted in Fig. 7. It clearly shows that the relative errors notably increase with  $F_{r1}$  for  $F_{r1} < 10$ . For most values of  $\tau_0/\tau_{w1}$ , the approximate results are greater than the numerical ones. In addition, the relative error increases with  $\lambda_1$  until it is over a certain value which is a function of  $F_{r1}$ , and then decrease to zero. The computation has shown that the relative error is smaller than 4% in the range of  $F_{r1} \leq 25$ . Therefore, Eq. (24) is a reasonable approximate formula for conjugate depths. If  $|\lambda_1 - 0.5| > 0.1$ , even in the situation where  $\eta$  is much greater than unity, accuracy can still be retained.

## 5 Verification of the formulas

An experimental investigation of hydraulic jump in Bingham fluid was conducted by Ogihara and Miyazawa (1994), who studied the flow in a rectangular open channel by using the mixtures of water and bentonite, which were regarded as Bingham fluid and observed that the characteristics of hydraulic jump in the Bingham fluid were not able to be fully described by the classical (Newtonian) hydraulic jump formulation. Their experimental results are adopted to verify the theoretical results in the present study.

A comparison between the theoretical results and the experimental data for conjugate depths is plotted in Fig. 8. It can be seen that the experimental data are scattered. This may be due to the difficulty to measure the conjugate depths in hydraulic jump. The agreement between them is reasonably good.

For critical depths, the results between the theoretical ones and the experimental data are also compared and plotted in Fig. 9. The figure has clearly shown that there is a good agreement between them.

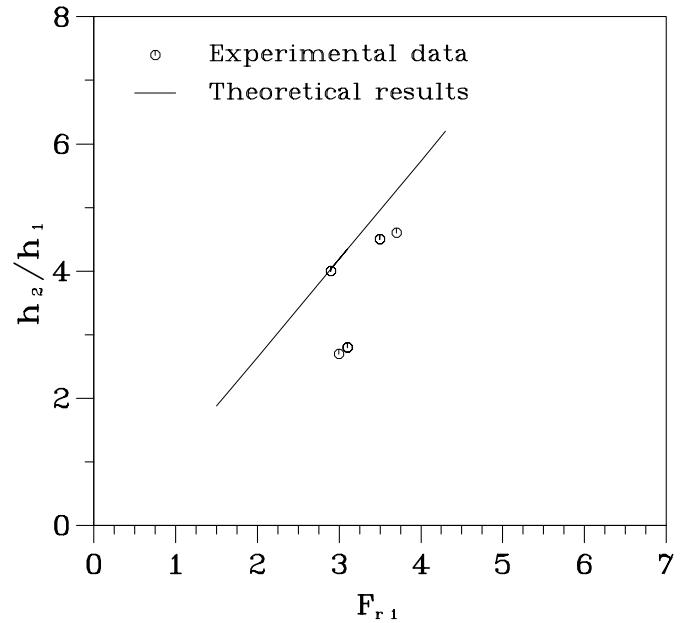


Figure 8 Comparison of the conjugate depth.

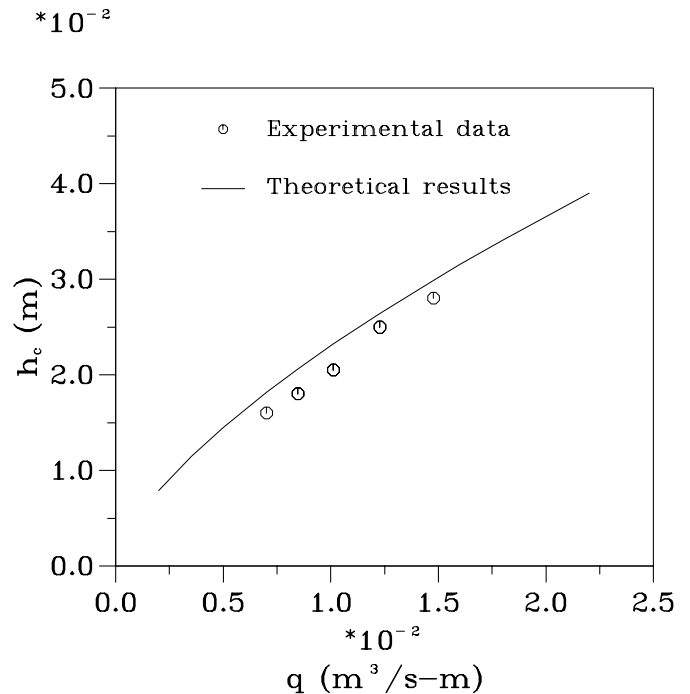


Figure 9 Comparison of the critical depth.

In addition, the critical depth increased dramatically was reported by Ogihara and Miyazawa (1994), when the dimensionless yield stress  $\lambda$  exceeded 0.1 in the experiment. This supports the theoretical result from the present study because  $h_c$  increases with  $\lambda$  in the range of  $0 \leq \lambda \leq 0.213$ . As indicated in Section 3, the critical depth continues to increase up to  $\lambda = 0.213$ . After that, it decreases with  $\lambda$ . Unfortunately, in the experiments, there is no further result available for this comparison.

## 6 Conclusions

The formulas for conjugate depths, bottom shear stress and critical depth have been derived. The critical depth reaches the

maximum at  $\lambda = 0.213$  where the critical flow is coupled between the effects of plug and shear regions. The bottom shear stress  $\tau_{w2}$  is always smaller than  $\tau_{w1}$ . Also, the approximate formula for conjugate depths with good accuracy is developed. The results are consistent with fully viscous or fully inviscid flows when  $\lambda = 0$  or 1, respectively. The verification of the formulas is carried out by a comparison between the theoretical results and the experimental data. It has shown that the agreement is reasonably good. The formula also indicates that there is an apparent increase of critical depth for  $\tau_0/\tau_w \leq 0.213$ , which has been supported by the experimental observation that critical depth increased greatly for  $\tau_0/\tau_w \geq 0.1$ .

### Notation

|                   |   |
|-------------------|---|
| $F_r$             | = Froude number                         |
| $g$               | = Acceleration due to gravity           |
| $h$               | = Conjugate depth                       |
| $h_c$             | = Critical depth                        |
| $h_q$             | = Critical depth in fully inviscid flow |
| $p$               | = Pressure                              |
| $q$               | = Discharge per width                   |
| $U, U_0, \bar{V}$ | = Velocity                              |
| $V_0$             | = Depth-averaged velocity               |
| $x, y$            | = Cartesian coordinates                 |
| $\Delta H$        | = Head loss                             |
| $\eta$            | = Ratio of conjugate depths             |
| $\lambda$         | = Dimensionless yield stress            |
| $\mu_0$           | = Viscosity coefficient                 |
| $\xi$             | = Dimensionless coordinate              |
| $\rho$            | = Density                               |

|          |                       |
|----------|-----------------------|
| $\tau$   | = Stress              |
| $\tau_0$ | = Yield stress        |
| $\tau_w$ | = Bottom shear stress |

### Subscript

1, 2 = Upstream, downstream

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